

IN THE CLAIMS

Please amend the claims as follows:

Claim 1 (Currently Amended): A process for preparing hydrocyanic acid (HCN) comprising:

catalytically dehydrating gaseous formamide in the presence of atmospheric oxygen in a reactor comprising an inner reactor surface comprising a steel comprising iron and chromium and nickel;

wherein:

the process is carried out at a pressure of from 200 to 250 mbar; and wherein

the reactor contains no additional internals, catalysts, or ~~a combination~~combinations thereof.

Claim 2 (Canceled)

Claim 3 (Previously Presented): The process of claim 1, wherein the steel comprises nickel and chromium in a ratio of from 1:1 to 1:2.

Claim 4 (Previously Presented): The process of claim 1, wherein the inner reactor surface comprises a steel comprising > 60% by weight of iron.

Claim 5 (Previously Presented): The process of claim 1, wherein the pressure/load ratio is from 1 to 100 kg of formamide/m² of reactor surface.

Claim 6 (Previously Presented): The process of claim 1, wherein the preparation of hydrocyanic acid is carried out in the presence of from 10 to 50 standard l of air/kg of formamide.

Claim 7 (Currently Amended): The process of claim 1 carried out at from 350 to 650°C.

Claim 8 (Previously Presented): The process of claim 1, wherein the reactor is a tube reactor comprising at least one tube.

Claims 9-13 (Canceled)

Claim 14 (Previously Presented): The process of claim 1, wherein the process is carried out at a temperature of from 500 to 550°C.

Claim 15 (Previously Presented): The process as claimed in claim 3, wherein the inner reactor surface comprises a steel comprising \geq 60% by weight of iron.

Claim 16 (Previously Presented): The process of claim 3, wherein the pressure/load ratio is from 1 to 100 kg of formamide/m² of reactor surface.

Claim 17 (Previously Presented): The process of claim 4, wherein the pressure/load ratio is from 1 to 100 kg of formamide/m² of reactor surface.

Claim 18 (Previously Presented): The process of claim 1, wherein the pressure/load ratio is from 5 to 80 kg of formamide/m² of reactor surface.

Claim 19 (Previously Presented): The process of claim 3, wherein the pressure/load ratio is from 5 to 80 kg of formamide/m² of reactor surface.

Claim 20 (Previously Presented): The process of claim 4, wherein the pressure/load ratio is from 5 to 80 kg of formamide/m² of reactor surface.

Claim 21 (Previously Presented): The process of claim 3, wherein the preparation of hydrocyanic acid is carried out in the presence of from 10 to 50 standard l of air/kg of formamide.

Claim 22 (Previously Presented): The process of claim 4, wherein the preparation of hydrocyanic acid is carried out in the presence of from 10 to 50 standard l of air/kg of formamide.

Claim 23 (Previously Presented): The process of claim 5, wherein the preparation of hydrocyanic acid is carried out in the presence of from 10 to 50 standard l of air/kg of formamide.

Claim 24 (Previously Presented): The process of claim 3 carried out at from 350 to 650°C.

Claim 25 (Previously Presented): The process of claim 4 carried out at from 350 to 650°C.

Claim 26 (Previously Presented): The process of claim 5 carried out at from 350 to 650°C.

Claim 27 (New): The process of claim 1, wherein the gaseous formamide is free from added inert gases and ammonia.